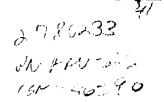


PRELIMINARY DESIGN REPORT



WASTEWATER TREATMENT FACILITIES

IRBID MUNICIPAL
WATER DISTRIBUTION,
SEWERAGE, STORM
DRAINAGE AND
SOLID WASTE
DISPOSAL PROJECT

SUBMITTED THRU

MINISTRY OF MUNICIPAL, RURAL AND ENVIRONMENTAL AFFAIRS - EXECUTING AGENCY

TO THE

NATIONAL PLANNING COUNCIL - THE HASHEMITE KINGDOM OF JORDAN

November 1980

By WESTON INTERNATIONAL, INC.

in association with STANLEY CONSULTANTS, INC. SIGMA-CONSULTING ENGINEERS MRM-CONSULTING ENGINEERS CO., LTD.

PRELIMINARY DESIGN REPORT WASTEWATER TREATMENT FACILITIES

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PRELIMINARY DESIGN REPORT

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908

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210

300

700

1.0 INTRODUCTION

In May 1979, the National Planning Council (NPC) of Jordan, through its executing agency, the Ministry of Municipal, Rural and Environmental Affairs (MMREA), gave authority to proceed with the feasibility and preliminary engineering phase of this project. The consultant group selected by NPC to provide services was WESTON INTERNATIONAL, INC., with its subcontractors; Stanley Consultants, Inc.; Sigma - Consulting Engineers, and MRM Consulting Engineers Co., Ltd.

A draft feasibility and preliminary engineering studies report was submitted in October 1979. The report was revised and resubmitted in March 1980. Additional comments were addressed and additional analyses were discussed in a report addendum submitted in August 1980. In September 1980 MMREA gave authority to proceed with Stage 2, detailed design of the facilities recommended in the feasibility study.

Major recommendations for wastewater treatment facilities contained in the feasibility report, as approved, include:

- Construction of an activated sludge wastewater treatment plant in the northeast portion of the Irbid Town planning area, adjacent to the existing municipal slaughterhouse.
- Construction of sand drying beds in an area north of the proposed treatment plant to dewater sludges produced by the treatment process.
- Construction of wastewater treatment facilities recommended to serve the needs of the City through the year 2000 in three implementation phases. One-third of the recommended treatment capacity is to be constructed immediately, followed by construction of the second third in 1985 and the remaining third in 1990.

This preliminary design report culminates the first step of the design process. The report sets forth the design criteria, provides a description of the wastewater treatment and sludge handling processes to be designed, and provides preliminary design drawings.

2.0 DESIGN OBJECTIVES

Peak Hourly Flow:

2.1 Design Flows

The proposed Irbid Municipal Wastewater Treatment Facility is designed to treat the anticipated flow from the Irbid town plan area through the year 2000. This objective is to be met in two phases; (1) construction of the facilities required to treat anticipated wastewater flows through the year 1990 and (2) construction of the facilities required to treat anticipated wastewater flows through the design year, 2000. In addition, bid packages will be prepared to allow contracting and construction of the facilities required for Phase I in two stages. Listed below is a summary of the flows which the wastewater treatment facility is being designed to treat:

	Flows (cubic meters per day,		$day, m^3/D)$
	Phas Stage 1	se I Stage 2	Phase II
Average Daily Flows:	11,023	22,046	35,852

30,146

60,293

95,580

The peak hourly flows include an allowance for infiltration and inflow from the proposed sanitary sewer system.

Provision is made in the proposed facility to receive and treat septage. Septage will be collected from tank trucks and metered into the wastewater flow stream at a constant rate. It is assumed that septage hauling volumes during the summer will be twice as great as the hauling volume during the winter months. The design allowances for septage are as follows:

	Quantity (c	ubic meters per	day, m^3/D)
Year	1990	2000	
Summer	713	1,086	
Winter	352	535	

These rates allow for treatment of septage from the unsewered areas within the Irbid town plan area as well as areas in the Irbid subdistrict outside of the town plan area.

2.2 Effluent Criteria

The treated effluent from the Irbid wastewater treatment facility will be discharged to the riverine system of the Wadi El Arab. The treated effluent will constitute a significant portion of the total flo. to the Wadi Arab reservoir. The reservoir will be used for irrigation and possibly livestock watering.

The proposed effluent standards for the Irbid wastewater treatment facility are tabulated below.

SUGGESTED EFFLUENT LIMITATIONS

IRBID MUNICIPAL WASTEWATER TREATMENT PLANT

Parameter	7-Day Average	30-Day Average
BOD ₅	45 mg/L	30 mg/L
Suspended Solids	45 mg/L	30 mg/L
Dissolved Oxygen	3 mg/L	3 mg/L
рН	6 - 9	6 - 9
Chlorine Residual	1.0 mg/L	0.5 mg/L

2.3 Construction Phasing

The proposed wastewater treatment facilities and sewage collection system are based on providing sewerage services for all residences expected to be located within the Irbid town plan area by the year 2000. A phased construction plan with two distinct construction phases was developed to achieve this objective.

Phase I of the sewerage system master plan is the largest and costliest phase. It includes construction of two-thirds of the proposed wastewater treatment capacity as well as construction of major portions of the proposed interceptor sewers, three pump stations and trunk sewers, and associated lateral sewers required to provide sewer collection service to those areas of the City of Irbid with the most urgent need.

Because of the size and cost of the proposed Phase I program it has been divided into two implementation stages. The major elements of the waste treatment facility to be constructed in each implementation stage are as follows:

Phase I - Stage 1

- All general site work including roads, fencing, grading, yard lighting, and the operations building.
- All required preliminary treatment facilities including grit chambers, bar screens, and flow measurement.
- One-third of the septage storage.
- One-third of the aeration basins.
- Two of four clarifiers. Note that the feasibility report originally proposed three clarifiers for the year 2000 facilities, viz, two for year 1990, and a third for year 2000. However, since the Phase I facilities are to be constructed in two stages, it is proposed, for versatility, to provide four smaller clarifiers to meet year 2000 requirements. Two of these clarifiers will be constructed during this initial stage. The clarifiers will be identical in size and capacity.
- One-third of waste sludge storage.
- One-third of sand drying beds.
- All required chlorination and reaeration facilities.
- Primary electrical switchgear for Phases I and II.
- Transformers, secondary switchgear and standby generators for Phase I, Stages 1 and 2.
- Motor control centers for Phase I, Stage 1.

Phase I - Stage 2

- One-third of the septage storage
- One-third of aeration basins.
- One clarifier.
- One-third of waste sludge storage.
- One-third of sand drying beds.
- Motor control centers for Phase I, Stage 2.

Phase II

- One-third of the septage storage.
- One-third of aeration basins.
- One clarifier.
- One-third of waste sludge storage.
- One-third of sand drying beds.
- Transformers, secondary switchgear, standby generator and motor control center for Phase II.



IRBID WASTEWATER TREATMENT PLANT

PRELIMINARY CONCEPT DESIGN

PRESENTATION AGENDA

Time	Agenda Item	Ву
1000 - 1030	Introductions	Coffee & Donuts
1030 - 1045	Project Overview	J.P. Miller, P.E. President, Weston International, Inc.
1045 - 1100	Concept Design Summary	D.P. Hunsinger, P.E. Project Manager
1100 - 1200	Presentation of Concept Design	P.J. Higgins, P.E. Design Manager
1200 - 1300	Lunch	
1300 - 1400	Tour of Weston Facilities	B.S. Cushing, P.E. Director of Design
1400 - 1430	Presentation Summary	J.P. Miller, P.E. & Staff

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Charles Phala rodays late that 45days late.

Charles Net 1 Planning Corneil (NPC)

Connect by and Jan, 40

DEMINISTRATION (Copter-NPC wanted work minimised short hinther didn't litts it Demograt of financial auto-can made hard to videntance stoga it of Minimised. Thereto, Thereto II to 2000

Demenge plust use extended aerealin, simple mach. Conso Person regions little constructation, law maintenance Standay as 500-contractor for the A stown drain was Septem size board on water domand, collection's yster Masky gravily flaw Design accepted /10/50 - Pullim. eng port dene since then Commune to to NPC - early Doc. Final design - later Teb 1981 Countration OVSS Tre-gralef. - stant I on, 81- to meet mid-81 Pontroction beginning deto -Pricting 113RD participation (Stove Sordahley) 10 UTB Train I- 1010, filere with IBRD morry De phase country play med extra money by 1963 mills AID ced put in \$20 mill, head \$50 folat It sive degree of trained of effluent, beyond Zudy Degree for we as ioning the animal all april 20 cycle 220 V.

3.0 DESIGN CRITERIA

It is the intent of these criteria to provide an acceptable basis for final design; therefore, the codes, materials of construction, descriptions of structures and the design bases are listed below for review and comment by all affected parties. Additions and changes to these criteria shall be made, if required by design or code, as the work progresses.

3.1 Hydraulic Design Criteria

- A. All forward flow process piping is to be reinforced concrete pressure pipe or ductile iron, with head loss calculations based on "Williams and Hazen" "C" = 100 (old pipe), and pipes flowing full.
- B. Open flow channel head losses are calculated using "Manning's" formula "N" = 0.013.
- C. The hydraulic profile through the treatment process is based on 22,046 m /D which is the average 24 nour flow for the year 1990. All pipes and channels have been sized to handle 95,580 m /D, peak flow for year 2000.
- D. The plot plan has been developed for all the process equipment and tankage needed for the 1990 flows. Consideration has been given for future additions of tankage and equipment in the year 2000.

3.2 Mechanical Design Criteria

- A. Major process pressure piping is to be ductile iron, with flanged or victaulic couplings above grade and mechanical or push-on joints below grade.
- B. Drain piping is to be cast iron under all structures, with the plant drain system being reinforced concrete.
- C. Water piping is to be galvanized steel inside the building and galvanized steel or cast iron below grade.
- D. Heating, Ventilating, Air Conditioning (HVAC)
 - Process area is to be heated ':o 13° C.
 - Office and shop areas are to be heated to 20° C.

Design outside temperatures:

Winter: 0° C and wind speed of 24.1 kilometers per hour

Summer: 35° C wet bulb

- Process and shop areas, with the exception of the Chlorine Room, are to be ventilated at six air changes per hour (summer only).
- Chlorine Room is to be ventilated at twelve air changes per hour.
- E. Plumbing shall be in accordance with the Building Officials Code Administrators (BOCA) Plumbing Code.
- F. Head loss calculation for pumping systems is to be based on "Williams and Hazen" "C" = 100 (Old Pipe), plus 15% safety factor.
- G. Process tanks are to have dewatering drains or pumpout sumps.
- H. Mechanical equipment housed inside will be arranged to allow for means of mechanically lifting for purpose of removal.
- Mechanical equipment requiring routine maintenance will have a minimum of 60cm clearance on all sides.
- J. Sludge force main pipe will be steel, coated and wrapped for below-grade service.
- K. Emergency generator will be provided for major process equipment, in case of electrical power failure.

3.3 <u>Structural Design Criteria</u>

A. Codes

- General Basic Building Code, Seventh Edition 1978 by Building Officials Code Administrators, International, Inc. (BOCA), Chicago, Illinois, USA, 1980 Supplement.
- Reinforced Concrete All foundations are assumed to be spread footings or mat slab subject to the recommendations of the soils report.

- Hydraulic Structures Per ACI-318-63 "Building Code Requirements for Reinforced Concrete" and ACI-350R-77 "Concrete Sanitary Engineering Structures" (ACI- American Concrete Institute).
- Non-hydraulic structures Per ACI-318-77 "Building Code Requirements for Reinforced Concrete."

Note: Hydraulic structures include concrete tanks and other structures commonly used in water and waste treatment facilities where dense, impermeable concrete with high resistance to chemical attack is required.

- Structural Steel Per Manual of Steel Construction, Eighth Edition, American Institute of Steel Construction (AISC).
- Metal Deck Per Design Manual for Floor Decks and Roof Decks,
 Steel Deck Institute (SDI) Publication No. 23, 1978 Edition.
- American Society for Testing and Materials (ASTM), Latest Edition.
- Codes and Standards of National Fire Protection Association (NFPA), 1980 Edition.
- Any Local Codes which may have jurisdiction of requirements more stringent than the above codes (to be furnished by MMREA).

B. Materials/Strength

 Concrete: Minimum 28 day compressive strength, f'c - 3000 psi (20.7 MPa), batch mixed and delivered to the project site.

Batching facilities will require the review of the engineer for quality control of procedure and materials used to produce the concrete. Testing facilities will be required to monitor concrete mix during mix design and production. Concrete tests will be in accordance with current ASTM methods.

- Concrete Reinforcing Steel: ASTM-A615 "Deformed and Plain Billet -Steel Bars for Concrete Reinforcement" Grade 40; Yield 40,000 psi min. (276 MPa). Design Stress 20,000 psi Max. (138 MPa).
- Soils: To be determined upon receipt of soils investigation report.
- Cement Mortar: If locally manufactured of local materials, mortar will be in accordance with local specifications or laboratory test results; or: Per ASTM - C270 "Standard Specification for Mortar For Unit Masonry" (type shall be determined later dependent upon available materials).

- Concrete Masonry Units: If locally manufactured of local materials, masonry units will be in accordance with local specifications or laboratory test results; or: Per ASTM C90 "Standard Specifications for Hollow Load-Bearing Concrete Masonry Units"; per ASTM C129 "Standard Specifications for Non-Load-Bearing Concrete Masonry Units"; and per ASTM C145 "Standard Specification for Solid Load-Bearing Concrete Masonry Units."
- Structural Steel: Per ASTM A36 "Standard Specification for Structural Steel."

C. Live Loads

- Roof live load (snow or equivalent), minimum 20 psf (97.6 kgs per sq. m) on a roof slope having a rise not exceeding 4 (10.16cm) inches per foot (30.48cm).
- Floor Loading
 - Operations Building: General Live Load, minimum 100 psf (488.2 kgs per sq. m) plus major equipment. Maintenance area, 200 psf (976.4 kgs per sq. m).
 - Vibrating Equipment (unless otherwise recommended by equipment manufacturer), weight times impact factor.
 - Platforms and walkways, 75 psf (366.2 kgs per sq. m)
 plus any equipment weights, either temporary or permanent.
 Handrail and stair loads will be in accordance with minimum
 Occupational Safety and Health Administration (OSHA) standards.
 - No live load reductions will be applied.

D. Other Loads and Forces

- Foundation bearing value and active lateral earth pressure on vertical tank walls will be determined by the soils engineer upon review of the soils report.
- Wind load on vertical surfaces above finish grade, per basic building code, Table 712.1 subject to prevailing basic wind speed. Minimum wind pressure:

Less than 30 ft (9.14m) 20 psf (97.6 kgs per sq. m) 30' - 40' (9.14 - 12.2m) 25 psf (122.0 kgs per sq. m)

 Earthquake Loading: Assume not greater than Zone 1 (per Basic Building Code, Appendix L) - minor damage unless local experience or records do not show loss of life or property damage.

E. Building and Structure Descriptions

Operations Building and Miscellaneous Equipment Buildings.

Roof Construction - Insulated steel metal deck supported on steel sub-framing with built-up roofing membrane in accordance with recommendations of roofing system manufacturer.

Floor Construction - Concrete slab on sub-grade.

Foundations - Concrete

Exterior Wall Construction - Insulated sandwich metal wall supported on steel sub-framing.

Interior Walls - Hollow non-load bearing concrete block extending to above the ceiling line or to underside roof deck, or; prefabricated demountable partitions extending to underside of the ceiling.

Tanks and other miscellaneous structures.

Septage Tanks - Concrete slab and walls and cover - below grade.

Influent Structure and Flow Distribution Box - Concrete slab and walls, with polyvinyl chloride (PVC) Parshall Flume.

Electric Substation, Emergency Generator and Miscellaneous

Motor Control Centers - Concrete slab on grade with prefabricated steel structure similar to operations building.

Aeration Tanks - Multi-cell concrete construction with concrete slab, dividing, and exterior walls, and concrete bridge to each aerator support platform.

Flow Splitter Box to Clarifiers - Concrete slab and wall construction.

<u>Sludge Holding Tanks</u> - Multi-cell structures with concrete slab and walls.

Clarifiers - Concrete slab and walls with concrete launder trough - below grade.

<u>Chlorine Feed Facility</u> - Concrete slab on grade attached to or adjacent to the sludge holding tanks.

Chlorine Contact Tank and Flume with Cascade - Concrete slab and wall construction - below grade.

lή

3.4 <u>Electrical Design Criteria</u>

Electrical equipment will be designed and constructed according to NEMA or ANSI standards and carry U.L. labels where applicable. The electrical design will be in accordance with the 1981 Edition of the National Electrical Code.

The lighting design will incorporate energy efficient sources and the lighting levels will be in accordance with the latest recommendations of the U.S. Government to provide adequate lighting levels and conserve energy.

4.0 TREATMENT PROCESS DESCRIPTION

The Feasibility Report prepared for the City of Irbid recommends the design and construction of a new wastewater treatment plant to treat the city's sewage and septage. The new treatment facilities will utilize the activated sludge process to achieve the effluent limitation of 30 mg/L BOD and 30 mg/L suspended solids (based on a 30-day average) and will be designed to handle 22,046 m³/D average flow for the year 1990, with expanded flow of 35,852 m³/D in the year 2000. The plant's hydraulics and key process units have been designed for the future expansion, as well as for both summer and winter flow and loading conditions.

Influent to the plant will flow through two 1.22m mechanically-cleaned bar screens to remove bulk solids. The bar screens will discharge solids into dumpster type containers for disposal in the City landfill. Mechanical cleaning of the bar screens will be actuated by a timer or differential pressure switch. A 1.22m manually-cleaned bar screen is also provided. Slide gates will be used to isolate or direct the flow to any particular bar screen.

Following the bar screens, flow passes through an influent Parshall flume, used for measuring flow, and then into aerated grit chambers. Two grit chambers will be provided. Centrifugal blowers, located adjacent to the grit chambers, will be used to supply air, through a swing diffuser, to the grit chambers. The grit chambers will have sloped sides with a troughed bottom to allow for grit removal by a "clam shell" bucket supported from an overhead monorail system. Following the grit chambers, effluent discharges into Flow Box No. 1 which splits the forward flow into four streams, two each to tanks T-3 and T-4. The flow box has been designed to be readily modified for future expansion. Sluice gates will be provided on each line leaving the flow box to allow for isolation of the aeration tank (T-3 and T-4).

Two aeration tanks will be provided, each containing two rows of 6 cells, a total of 12 cells per tank. Each cell will operate in parallel and will contain a 100 horsepower platform mounted surface aerator, a foam spray system, and a sludge return sump with an inclined screw pump. The recycled sludge will flow by gravity from the return sludge well to the sump in each aeration cell where it will then be lifted approximately 2m, by a screw pump, and will discharge into the basin inlet. The screw pump flow rate will be adjustable by controlling the submergence of the feed end of the pump. This will allow for individual recycle flow control for each cell. Forward flow into cells will be by an external side trough feeding each row of six cells. Effluent from each cell will discharge into a central channel which flows to Flow Box No. 2. Each cell will have an adjustable influent and effluent weir.

Both aeration tanks will discharge into Flow Box No. 2, where the flow will be equally divided prior to flowing to the three clarifiers. Flow Box No. 2 is designed to allow for future addition of a fourth clarifier.

The clarifiers are 27.6m diameter and equipped with hydraulic sludge removal and scum removal mechanisms. Sludge from all clarifiers will be collected in the sludge return well, from which it will flow, by gravity, to each aeration cell. Waste sludge will also flow by gravity to the sludge holding tank screw lift pumps. These pumps will elevate the waste sludge to a center distribution channel and in turn into the holding tank.

The overflow from clarifiers will be combined in the chlorine mix tank where a 5 HP mechanical mixer will mix the wastewater with the chlorine solution. From the mix tank, the flow is split into two, end-around baffled, chlorine contact tanks. A pump well has been provided at the end of the chlorine contact tank for installation of both the spray water and utility water pumping systems. The spray water system will provide effluent water for foam control, if needed, in each aeration cell. Utility water will be used for chlorination and miscellaneous plant wash down. The utility water system will be a constant pressure system using vertical turbine pumps and regulating valves to maintain the pressure.

An effluent Parshall flume is used for flow measuring, prior to re-aeration. A cascade re-aerator chamber is provided to raise the effluent D.O. to more than 3 mg/L before discharging to the Wadi El Hamam.

Four sludge holding tanks are provided in Phase I and two additional holding tanks are provided in Phase II for waste sludge storage prior to transferring sludge to the drying bed site. Each tank will have a submerged turbine aeration system consisting of a platform mounted agrator and a bottom air sparger ring to provide mixing and to maintain dissolved oxygen in the tank. A package positive displacement blower will be mounted on the aerator platform to provide air for the sparger ring. A decant system is provided in each tank. Prior to pumping waste sludge to the drying beds, the mixer will be shutoff and clear supernatent will be returned to the aeration basins.

Sludge will be withdrawn from holding tanks and pumped across the road to the drying beds. Sludge pumping will be accomplished by the use of two triplex plunger pumps working in parallel. Two, 200mm diameter force mains will be provided to transport sludge to the drying beds. Although two pipes are provided only one will be used. The second is a complete spare to be utilized to relieve possible difficulties which can occur when pumping sludge a long distance. The pumping system is designed to be operated six days per week, twelve hours per day. The two force mains will be connected to create a loop and a waterflushing system, using plant effluent, will be provided to scour the pipes and minimize buildup of deposits. The flushing system will be manually connected at the completion of each pumping cycle.

Twenty-eight sludge drying beds will be provided for the year 1990, with a total of 42 for year 2000. Each bed will be 30m x 75m with 200mm of sand over 400mm of gravel. The beds will have a perforated P.V.C. piping network under the gravel to collect the "underdrainage" and will discharge in a lined earthen pond. The pond will also collect stormwater from the beds, and local runoff. Discharge from the pond will be by gravity back across the road to the treatment plant, discharging into the "Plant Drain Pumping Station" for conveyance to the head end of the treatment facilities. An adjustable slide gate will be used to control the rate of discharge from the pond.

Septage handling facilities have been provided to store the waste prior to pumping it, at a controlled rate, to the head end of the treatment facilities. The septage haulers will empty their trucks, by gravity, into one of two inground tanks to be provided for the Phase I facilities. (A third tank will be provided for Phase II.) Each tank will be covered, and equipped with a mechanical mixer. An odor control system will be provided on the tank vents to eliminate the possibility of offensive odors. Since the tanks are inground it will be necessary to pump the septage to the influent structure. This will be accomplished by using two screw pumps that lift the septage to an elevation from which it can flow by gravity to mix with the treatment plant influent. A coarse, manually cleaned, bar rack will be provided at the septage truck discharge manhole for removal of large solids.

The chlorination feed facilities will consist of two separate systems. One system will be a complete spare. The normally operating system will feed chlorine solution for disinfection. The spare system will be designed to allow for auxiliary chlorination at the septage holding tanks, influent structure, and/or return sludge system if necessary, as well as a back-up to the primary disinfection system. Each system will have a capacity of 800 kg/D and consist of an evaporator and chlorinator with a cabinet-mounted ejector. The chlorine feed rate will be paced automatically by the plant effluent flow rate. The chlorine facilities will be housed in the sludge transfer pumping station.

5.0 MAJOR EQUIPMENT LIST

INFLUENT BAR SCREEN ME la & b

Number Two Width 1.22m

Type Catenary, mechanical cleaned Remarks One manually cleaned

One manually cleaned bar screen to be provided as back-up to mechanical

cleaned

INFLUENT MEASUREMENT

Number One
Type Parshall
Size 900m

Construction Fiberglas flume cast in concrete channel

GRIT REMOVAL CHAMBER T-la & b

Number Two
Type Aerated

Size 3m wide x 10m long x 3m deep

Remarks Grit removal by overhead "clam shell"

AERATION GRIT BLOWERS ME 2a, b, c

Number Three
Type Centrifugal
Size 8.5 m³/min. each

SEPTAGE HOLDING TANK T-2a & b

Number Two and one future

Size (each) 9.15m x 9.15m x 3.05m SWD to 0.61m F.B. 255 m³

Construction Concre

Construction Concrete with cover Function To reactive and access

unction To receive and store septage prior to

pumping to treatment facilities.

SEPTAGE TRANSFER PUMPS P la & b

Mixer

Number
One operating and one spare and one future

Capacity

24-1 m3/hm

Capacity 24.1 m³/hr. Type Screw Purps

Type Screw Pumps
Size 365mm

365mm Lift 3.66c.

FLOW SPLITTER BOX FB-No. 1

Number Size

Construction

Function

AERATION BASIN P-3a to 31 P-4a to 41

> Number Dimension (each) Flow per Basin Detention Time Construction Remarks

AERATOR M-3a to 31 M-4a to 41

> Number Туре

Size Drive

Oxygen Requirements

Minimum D.O. Remarks

SLUDGE RECYCLE PUMPS P-3a to 31 P-4a to 41

> Number Type Flow Control Drive Size Function Remarks

One $6.70m \times 6.09m \times 3.65m$

Concrete

To split forward flow equally to six

aeration trains

24 and 12 future

 $16.55m \times 16.55m \times 3.75m \text{ SWD} + 1m \text{ F.B.}$ $948 \text{ m}^3/\text{D}$ Average yr. 1990

1 day @ average flow

Concrete

A total of three separate aeration structure for the year 2000 flows will be provided. Each structure will contain 12 aeration basins (two rows of 6 cells) with common effluent troughs. Each basin will contain a foam spray water system to control foam buildup.

24, one per cell Platform mounted mechanical surface aerators 100 HP each Single speed 132 Kg/hr. at standard condition 2 mg/L

Aerator will be supplied with baffles mounted on platform.

One per Aeration Cell. Total - 24 Screw Pumps 0 to $64.85 \text{ m}^3/\text{hr}$.

Adjustable Submergible device

3 HP constant speed

400mm Ø

To return sludge to each aeration cell. Sludge will be returned to a compartment within each aeration basin by gravity, from which the screw pump will take suction and will discharge to the basin inlet.

SPLITTER BOX FB No. 2

Number

Size

Construction

Function

One

 $6.70m \times 5.48m \times 3.65m$

Concrete

To collect the mixed liquor from the two aeration structures (three in the future) and equally split the flow to three (four in the future) clarifiers.

CLARIFIER T-5a, b, c

Number

Size

Construction

Three plus one future

27.44m Ø x 4.3m SWD + 0.60m FB

Concrete, inboard launders and scum pit.

CLARIFIER MECHANISMS ME-2a, b, c

Number

Type

Dr ive

One per tank, total of three

Center pier supported with hydraulic

sludge removal and scum skimming

One HP

SCUM PUMPS P-5a, b, c

Number

Size

Type

Total three (one per clarifier)

 $18 \text{ m}^3/\text{hr.}$ at 4.5m TDH

Submersible

SLUDGE RETURN WELL T-10

Number

Size

Construction

Function

One

 $6.0 \text{m} \times 4.0 \text{m} \times 4.0 \text{m}$

Concrete

To collect sludges from clarifiers and split return flow to aeration basin and serve as wet well for sludge wasting

pumps.

Remarks

Sludge return well will be constructed as part of FB - using common walls.

SLUDGE WASTING PUMPS P-9a & b

Number

Size

Type

Drive

Control

Capacity

Remarks

One operating plus one spare and one future

500mm

Screw

3 HP constant speed

Adjustable depth control

 $0 - 108 \, \text{m}^3/\text{hr}$.

Waste sludge will flow by gravity from sludge return well to lift station where 500mm screw pumps will lift to dig-

estors.

CHLORINE MIX TANK T-7

Number Size

Detention Time

Function

0ne

3m x 3m x 3.3m SWD + 0.60m FB 1 Min. @ Average Flow Yr. 2000 Provide mixing of chlorine solution and wastewater stream to insure dis-

infection.

CHLORINE MIXER M-2

Number Type Materials Drive Remarks

One.

Platform Mounted
Rubber coated steel
5 HP Constant speed

Chlorine solution to be introduced into mix tank through diffuser on bottom of

tank.

CHLORINE CONTACT TANK T-8a & b

Number Dimension (each) Detention Time @ Peak

Hydraulic Flow Construction

Two

 $17m \times 10.5m \times 3.3m \text{ SWD} + 0.60m \text{ FB}$

15 Min.

Concrete with end around baffle walls.

CHLORINE FEED SYSTEM ME 200 & 201

Number of Systems Capacity per System Dosage Rate Chlorine Supply

Size

Two

800 Kg/Day 8 mg/L

Ton cylinders

Evaporator ME 200b & 201b

Number Capacity Type

One per system 800 Kg/Day Cabinet mounted

Chlorinator ME 200c & 201c

Number Capacity · Type

One per system 800 Kg/Day Cabinet mounted

Remarks

One chlorination system will be used for disinfection, with the spare system being used for pre-chlorination and septage chlorination, if necessary. The chlorine feed system will be housed in the sludge transfer pumping station.

CHLORINE CONTACT TANK PUMP SUMP T-9

Number One

Size $10m \times 3m \times 3.3m \text{ SWD} + 0.6m \text{ FB}$

Construction Concrete

Function Provide wet well for foam spray water

pumps and utility water pumps.

FOAM SPRAY WATER PUMPS P-7a & b

Number One operating and one spare

Size $306 \text{ m}^3/\text{hr. x } 10 \text{m } \text{TDH}$ Type Wet well centrifugal
Drive 20 HP constant speed

Function To provide spray water for foam control

in aeration basins.

UTILITY WATER PUMPING SYSTEM P-8a & b

Size 45.4 m³/hr. @ 45m TDH

Number of Pumps One operating and one spare

Type Vertical wet pit, constant pressure

system.

Drive 10 HP constant speed

EFFLUENT MEASUREMENT

Number One Size 9.0mm

Type Parshall flume

Construction Fiberglass flume cast in concrete channel.

REAERATION STRUCTURE

Number One

Type Stepped cascade

Vertical Drop 4.27m D.O. Increase 3.0 mg/L

Function To reaerate effluent to 6.0 mg/L before

discharging to the Wadi.

PLANT DRAIN PUMPING STATION P-2a & b

Number of Pumps Two Capacity $90 \text{ m}^3/\text{hr}$.

Type Wet well/dry well

Wet Well Size $2m \notin x \cdot 3.75m$ Deep Function

ction To receive & transfer discharge from internal Plant Drain System and overflow from "Storm water & Sludge Drying Bed

Drive Underdrain Basin"
10 HP constant speed

Construction Concrete

SLUDGE HOLDING TANK T-11a, b, c & d

Number 4 and 2 future

Size $16.55 \text{m} \times 16.55 \text{m} \times 3.75 \text{m} \text{ SWD} + 1 \text{m} \text{ FB}$

Volume 1027 m³
Construction Concrete

Construction Concrete/common walls
Function To store and thicken (by decanting)

waste sludge prior to pumping to sludge

drying beds.

AERATORS M-5a, b, c & d

Number One per tank, total of 4

Type Platform mounted submerged turbine, with

air blowers

Drive 15 HP constant speed

AERATION BLOWER ME-4a, b, c & d

Number

Type Positive displacement

Capacity 20 m³/Min

Drive 20 HP Constant speed

SLUDGE TRANSFER PUMPS P-6a, b & c

Number Two operating and one spare

Capacity (each)

Type

Plunger - triplex

Orive

40 HP constant speed

Function To transfer sludge from holding tank to

sludge drying bed site.

SLUDGE FORCE MAIN

 $\begin{array}{cc} \text{Number} & \text{Two} \\ \text{Size} & \text{200mm} \\ \text{Materials} & \text{Steel} \end{array}$

Length Steel 1000m

SLUDGE DRYING BED

Number Yr. 1990 28

Yr • 2000 42

Size $30m \times 75m$

Construction Concrete wall with sand and gravel base.

Bed will have piped under drain system

and will be compartmented.

STORM WATER AND UNDER DRAIN POND

Number
Size @ Top
Side Slope
Capacity
Eff. Control
Construction
Function

One
37.64m x 37.64m x 3m SWD + 0.6m FB
2:1
2270 m³
Adjustable slide gates
Earthen with liner
To store sludge bed under drain and storm runoff prior to transfer to wastewater treatment plant.

6.0 ELECTRICAL/INSTRUMENTATION

6.1 Electrical Distribution

The electrical system will provide reliable power to operate the wastewater treatment plant's mechanical equipment. The system to be installed in Stage 1 of Phase I will have capacity to power the equipment installed under the two current bid packages (Stages 1 and 2) and in addition there will be primary switchgear capacity for the planned expansion (Phase II) for the year 2000.

Electrical power will be received from the utility company at 11.33 KV, 30, 50 Hz on the south side (Irbid side) of the wastewater treatment plant. The utility company will provide power via an aerial line and will extend it to within fifteen meters of the primary switchgear. The service and primary switchgear will be designed to handle the year 2000 power requirement which is 4300 KVA.

The primary switchgear will consist of a line-up of 15 KV fused load break switches. The line-up will be "non-walk-in type" outdoor switchgear as manufactured. There will be a main fused load break switch and lightning arrestors, utility company metering compartment, two feeder compartments each with fused load break switches and space for a future feeder compartment.

Each feeder compartment will feed a 1500 KVA, 30, 50 Hz, OA-FA rated transformer. The transformer will be connected Δ -Y4 with a secondary voltage of 380, 30, 50 Hz. The transformers will be of the oil type and located outdoors.

Immediately adjacent to the transformers will be the line-up of 380 volt secondary switchgear. The switchgear will be of the outdoor walk-in type and be connected to the transformer by means of 3000 ampere enclosed busway. There will be a main breaker rated 3000 amperes surge, and lightning protection, and four feeder breakers rated 800 ampere. The breakers will be draw-out air type with static trips including ground fault protection. The feeder breakers will be of the fused type to limit fault currents available to downstream devices. Downstream of the main breaker will be an automatic transfer switch rated 3000 amperes to transfer automatically to standby power on a loss of utility service power.

Standby power will be provided by 840 KW diesel generating sets. There will be one set for each lineup of secondary switchgear. These sets will provide enough power to maintain flow through the plant and provide adequate treatment during the temporary outages. Temporary power will be provided to handle the following loads:

QUANTITY	DESCRIPTION
1	Bar Screen
1	Grit Blower
12	Aerators
3	Clarifiers
1	Chlorinator
2	Septage Mixers
2	Sludge Holding Tank Mixers
2	Sludge Holding Tank Aeration Blowers
12	Sludge Recycle Pumps
1	Chlorine Mixer
1 .	Plant Drain System Pump Station
	Operations Building Power and Lighting

Each of the secondary switchgear feeder breakers will feed a motor control center rated 800 amperes at 380 volts, 30, 50 Hz. The motor control centers will be located in the electrical room at the operations building. Power will be supplied to equipment motors through combination motor starters in the motor control centers. The combination motor starters will consist of fused disconnect switches in conjunction with magnetic contactors.

All electrical equipment will be designed according to NEMA or ANSI standards and carry U.L. labels where applicable. The electrical design will be in accordance with the 1981 Edition of the National Electrical code. The largest motors at the facility are the aerator motors which are 100 HP. These motors will be started using autotransformer reduced voltage motor starters. The use of these starters will reduce the inrush on start-up of the equipment and will allow the use of smaller standby generators.

Illumination in the operations building will be provided through the use of fluorescent fixtures with energy efficient lamps and ballasts.

The exterior lighting will be through the use of high pressure sodium fixtures controlled either by timers or photo cells.

The sludge drying beds, which are located approximately 1200 meters from the treatment plant, will also be lighted. A separate service from the utility company will be provided. This service will be of the secondary type at 220 volts, 10, 50 Hz. A local weatherproof switching center will be provided. The total load for the present and future lighting at this site will be approximately 20 KW.

6.2 Instrumentation

The basic instrumentation philosophy is simplicity through metering and manual process control.

Influent flow is measured by a Parshall flume. The head representing flow is sensed by a non-contacting (sonic) transducer. The transducer output is converted to a unit of flow. A local readout in flow and head are provided at the flume. Signals proportional to flow rate are integrated, totalized, and transmitted to the main control panel where they are displayed on a recorder and counter respectively. The main control panel will be located in the operations building.

Effluent flow is measured in the same manner, and is recorded and totalized. The effluent flow rate signal is re-transmitted to the chlorinator for use as a pacing signal. The pacing signal proportions the chlorine flow rate to effluent flow. The ratio of chlorine to flow is determined from a grab sample and lab test.

Septage and plant drain recycle flow is measured by flumes recorded and totalized similiar to Plant influent.

Liquid levels are sensed and alarms activated when they exceed set maximum values in the following locations: 1) upstream channel of each bar screen; b) clarifier scum pits; and c) plant utility water well.

Operation alarms are provided to warn of a malfunction of the following equipment:

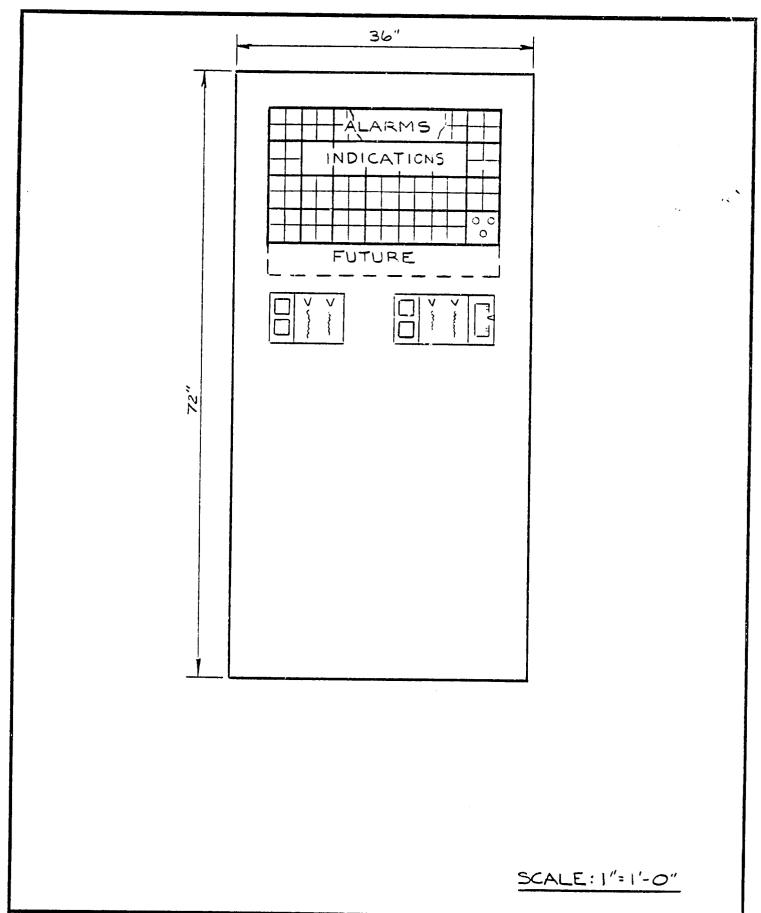
- Mechanized Bar Screens
- Clarifiers (high torque)
- Chlorine Systems.

Operation of all of the primary equipment is monitored and indication of its status (off or on) is displayed on the main control panel.

 $\sqrt{1}$

The main control panel is for monitoring only with no control from this point. The monitoring consists of alarm functions, status monitoring of equipment operation, recording of influent and effluent flow rate, flow totalizing, and chlorine ratio setting. The panel layout is shown on the next page.

Sludge recycle flow is controlled manually by positioning each screw pump discharge end and checking the discharge rate by manual measurement of flow over a weir. Activated sludge waste rates are controlled by time meters on the waste sludge pumps. Dissolved oxygen (D.O.) in each aeration basin will be measured with a portable unit as required.



WASTEWATER TREATMENT

FACILITIES

PROCESS MONITORING

PANEL

PROMITE DESCRIPTION DATE

PROVINCE DESCRIPTION DATE

OF ANY F. WESTON, INC.

ON F. WE

K&E 19 1253 6-80 MC11110

7.0 BUILDING RECOMMENDATIONS

7.1 Operations Building

The single story prefabricated steel building will be a steel sandwich wall panel and insulated roof panel construction connected to a steel frame, designed to sustain all design loads including wind, roof loads (such as snow or equivalent), lighting and piping loads, ceiling loads, and building heating and ventilating equipment loads, if any. The building foundation will be primarily a slab on grade with perimeter grade beams, subject to the recommendations of the soils report. Any major interior equipment will be founded on individual foundations.

Benefits to be derived from use of a prefabricated steel building include:

- 1. Rapid erection time once foundations are in place
- 2 The use of an enclosed area for storage of other equipment as delivered to the site;
- 3. The structure would be provided by a sole supplier and erected complete in place by a contractor acquainted with that type of construction and recognized by the supplier.

The building package would be specified to be furnished and erected by a sole supplier and his agent/erector to include all required materials and hardware. The building will be designed to be readily available through various prefabricated building manufacturers as sole supplier.

7.2 Plant Equipment Foundations and Process Tankage

Materials of construction for equipment foundations and process tankage will be poured-in-place concrete with steel reinforcement placed in form-work and constructed to the dimensions shown on the engineering drawings.

The site will be graded as required to provide the required grades above the equipment foundations and process tankage. Excavations will be made to elevations shown for bottom of concrete foundations.

7.3 <u>Miscellaneous Equipment Enclosures</u>

Miscellaneous equipment enclosures will be specified to provide weather protection and general security to such equipment that may have need for protection. Equipment, set on individual concrete foundations, will include, but not be limited to, process pumps, blowers, electrical substations and motor control centers, located in the vicinity of process tanks and miscellaneous equipment.

The enclosures will be prefabricated steel construction to match, as closely as possible, the finish of the operations building. The enclosure will be designed to sustain the same loading as the operations building, and will be secured to the concrete foundation for the equipment.

8.0 IRBID SPECIFICATIONS LIST (PRELIMINARY)

Section	<u>Title</u>
00700	General Conditions
00800	Supplementary Conditions
01010	Summary of Work
01011	Drawings
01015	General Conduct of Work
01080	Applicable Codes
01090	Abbreviations
01100	Substitution of Equipment and Materials
01150	Measurement and Payment
01300	Construction Progress and Schedules
01330	Survey Data
01340	Shop Drawings, Samples and Project Data
01400	Quality Control
01500	Temporary Facilities
01560	Maintenance of Work Site
01562	Dust Control
01580	Project Identification
01600	Materials and Equipment
01710	Cleaning Up
01730	Operation and Maintenance Data
02102	Grubbing and Stripping
02220	Excavation and Backfill

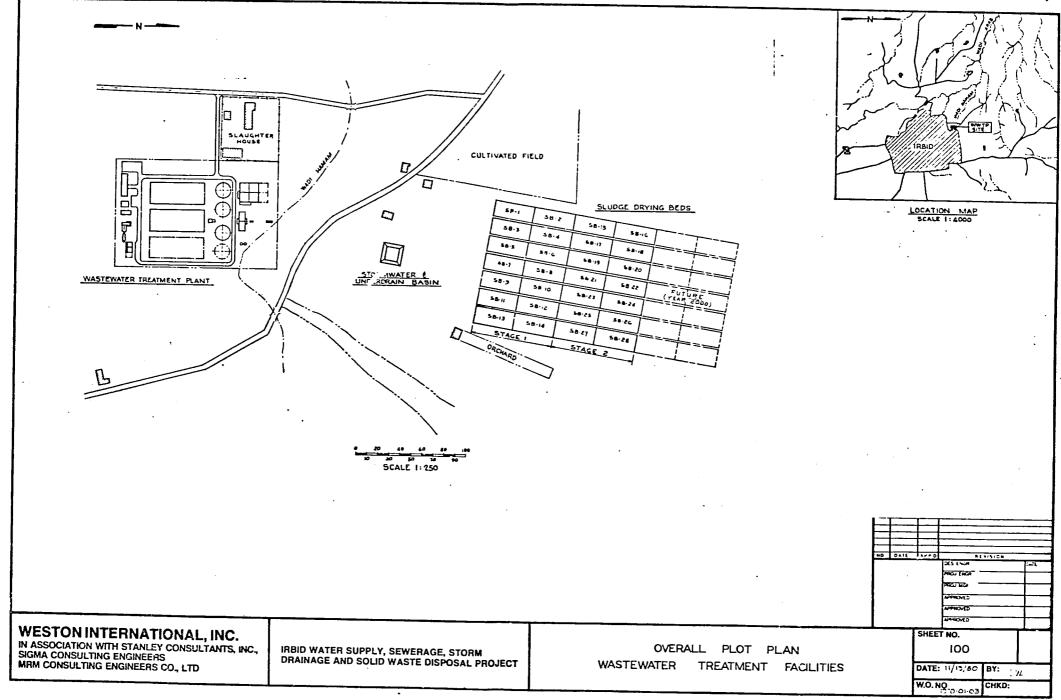
Section	Title
02260	Screened Gravel
02280	Crushed Gravel
02290	Selected Backfill
02540	Erosion Control
02575	Manholes
02612	Bituminous Paving
02711	Chain Link Fence
02820	Lawns and Planting
02821	Seeding
03100	Concrete Formwork
03200	Concrete Reinforcement
03300	Cast-in-Place Concrete
03315	Sanitary Structure Concrete
03600	Grout
04100	Mortar
04200	Masonry
05120	Structural Steel
05500	Miscellaneous Metals
06100	Rough Carpentry
07160	Bituminous Dampproofing
07951	Sealants and Caulking
08210	Doors and Door Frames
08360	Overhead Doors

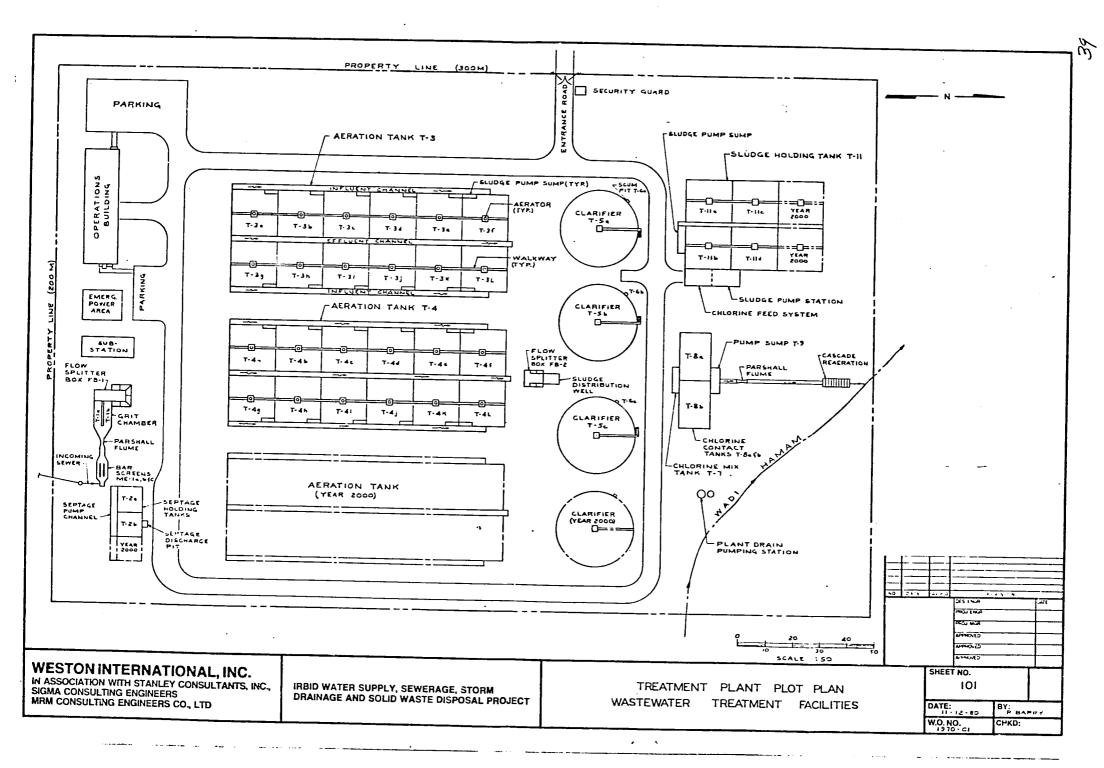
Section	<u>Title</u>
08710	Finish Hardware
08800	Glass and Glazing
0931Ó	Ceramic Tile
09330	Quarry Tile
09650	Resilient Flooring
09900	Painting and Coatings
10165	Toilet and Shower Compartments
10166	Toilet Room Accessories
10390	Miscellaneous Specialties
10500	Metal Lockers and Benches
11010	Mechanical Equipment - General
11061	Screw Pumps
11062	Centrifugal Pumps
11063	Plunger Pumps
11065	Submersible Pumps
11071	Mechanical Bar Screens
11075	Aerated Grit Removal System
11080	Mechanical Aerators
11083	Blowers
11160	Slide and Sluice Gates
11260	Chlorination System

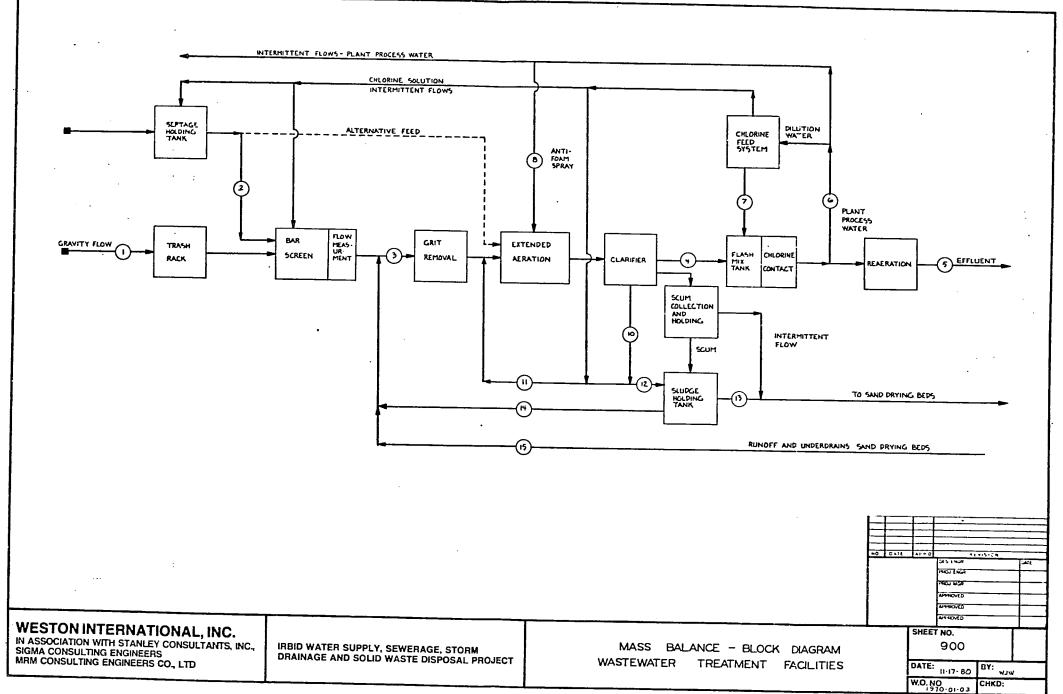
Section	<u>Title</u>
11373	Centrifugal Blowers
11550	Tools and Equipment
11600	Laboratory Equipment
11866	Conveyors
11930	Utility Water System
11945	Mixers
11953	Final Clarifiers
12610	Office Furniture
13120	Prefabricated Building
13440	Instrumentation - General
13441	Instrumentation Functional Descriptions
13442	Instrumentation Equipment
13443	Instrument and Control Panel
13444	Field Instrumentation Installation
14300	Monorail and Hoist Equipment
14560	Utility Vehicles
15010	Mechanical General
15050	Piping Material Classifications
15060	Piping Installation
15173	Flow Measuring Devices
15400	Plumbing
15450	Plumbing Fixtures

Section	Title
15800	Heating, Ventilating and Air Conditioning
16000	Electrical Work
16010	Electrical General
16050	Typical Details - Electrical and Instrumentation
16111	Conduit
16114	Cable Tray
16120	Wire and Cable
16131	Pull, Junction, Termination Boxes and Wiring Troughs
16134	Panelboards
16140	Switches and Receptacles
16150	Low Voltage Induction Motors
16160	Dry Type Transformers
16210	Generating Sets
16310	Substations
16320	Switchgear
16450	Grounding
16500	Lighting Fixtures and Lamps
16920	Motor Control Centers
	Electrical System Control Devices

Manholes and Handholes







WINTER CONDITION

STREAM NO		(2)	(3)	0	(3)	(3)	(3)	1 7
AVERAGE FLOW m3/	24Y 22 046	352			1	_\'	(i)	(•
PEAK HYD. FLOW =3,0		352	24 023 82 295	27.041	22 170	5.416	545	4 87
MIN. FLOW #3,0		352		67.166	82.285	5.416	545	4 17
TSS mg/L		2.349	9,170	9,170	9.170	545	545	
ISS Ag/d		827	899	20	20	20	20	7
125 mg/L		500	21.606	541	443	108		
SS hg/d		176	559 15,834		14	14	14	1.
1005 =g/L		4.801	810	379	310	76		
005 kg/d	87 17,742	1,590	19,447	20	20	20	20	2
X		 	12.447	541	443	108	11	1
.0.					6.8			
					3.0			

STREAM NO.	(10)	(11)	(12)	(13)	(14)	(15)
AVERAGE FLOW m3/day	28.059	26.206	1,853	1		
PEAK FLOW m3/day	35,405	35,405		1,235	E18	1,007
MINIMUM FLOW #3/day	T	1				1.850
DESIGN ISS &	1.0	10			0	0
DESIGN TSS mg L	10,000	10.000	1.0	1.5	.07	:
DESIGN ISS kg/day	280.590	262.060	10,000	14,600	741	22
GESTON VSS &	6.7	0.7		IE.074	458	22
DESIGN YSS SE/L	7,000	7,000	0.7	1.02	. 35	
DESIGN YSS kg/day			7.000	10.200	519	15
	188,413	193,442	12,972	12.851	321	15

SUMMER CONDITION

STREAM NO.		(1)	(2)	(3)	(1)	(5)	(0)		
EVERAGE FLOW	=3/DAY	22.046	713	1 200	<u> </u>	1		$\underline{}$	
EAK HYD FLOW	m3, DAY	55,115	713	24,552	27,300	22,509	5,418	545	4 871
IN. FLOW	m3/DAY	8 619	713	58,825 9,531	81.496	56.825	5,416	545	4.871
22	Fg/L	941	2.350		9,531	0,531	545	545	0
55	hg/day	20, 299	1,676	22,48*	20	20	20	20	20
55	mg/L	662	500	†···	546	450	108	11	87
22	kg/day	15,355	356	15.077	14	14	14	14	14
	Og/L	105	4.400	863	343	3:5	78		38
305	hg/day	17.742	3.442	21,180	20	25	20	20	20
<u> </u>					548	450	108	11	\$7
.0.				t		6.9			
						3.0			

STREAM NO.		(10)	(11)	(12)	(13)	(14)	(15
AVERAGE FLOW	m ³ /day	28,671	26.628	2,043	1,362	681	
PEAK FLOW	m3/cay	36.057	36 067				1,112
RINIMUM FLCA	m3/day	· ·				0	1,850
DESIGN TSS	1	1.9	1.0		<u> </u>		8
DESIDE 755	az/L	10,000		1.0	1.5	. 07	-
221 1431230	kg/day		10.000	10.000	14,600	711	22
DESIGN YSS	1	286.710	268.628	20,433	19,949	484	74
		0 7	0 1	0 7	1.02	.05	
DEZIEN AZZ	■g/L	7.000	7.000	7,000	10,200		<u> </u>
DESIGN VSS	kg/day	200,697	186,640	14,303	13,964	498	15

WESTON INTERNATIONAL, INC.
IN ASSOCIATION WITH STANLEY CONSULTANTS, INC.,
SIGMA CONSULTING ENGINEERS
MRM CONSULTING ENGINEERS CO., LTD

IRBID WATER SUPPLY, SEWERAGE, STORM DRAINAGE AND SOLID WASTE DISPOSAL PROJECT

MASS BALANCE - SCHEDULE I (YR. 1990) WASTEWATER TREATMENT FACILITIES

PHOU ENGA PROJ MOR APPONES. 4 THENED SHEET NO. 901 BY: W.O. NO

WINTER CONDITION

STREAM NO.			(2)	(1)	(•)	(3)	(i)	0	
AVERAGE FLOW	a3.DAY	35.852	713	39.126	43,548	36,239		<u> </u>	 ''.
PEAR HTD. FLOW		95.580	113	97.765	105.074	97,765	7,854	545	7.30
IIN. FLOW	m3 GAT	14,341	713	15.054	15.054	15,054		545	7.30
55	mg L	887	1.763	860	20	20	545 20	545	
22	kg/day	31,527	1.257	33 532	871	725	157	20	
\$\$	mg.L	567	374	630	14	14	14		14
55	kg day	23,928	267	24.651	610	597	110	14	
005	#g/L	762	3,602	765	20	20	20	20	10
005	kg/day	27,317	7,568	29.915	871	725	157	11	2
						6.9			14
.0.						3.0			

STREAM NO.		(10)	(1)	(12)	(13)	(14)	(15
	e3/day	45,688	42,781	2,887	1.924	963	1.598
	æ3/day	57,646	57.848	0	0	0	1.850
SINIBUM FLOW	<u>a3/day</u>				-	-	
DESIGN TSS	<u>s</u>	1.0	1.0	1.6	1 5		
DESIGN TSS	mg L	10,000	10,000	10,000	14,600	.07	
DESIGN TSS	1g/42y	456,680	427.810	28,868		736	22
DESIGN VSS	5	9.7	0.7	0.7	28,157	709	35
DESIGN YSS	■g/L	7,000	7.000		1.02	Q5	<u> </u>
			7.000	7.000	10.200	515	15

SUMMER CONDITION

STREAM NO.		(י)	(2)	; (<u>3</u>)	(1)	(3)	(1)		
VERAGE FLOR		35.852	1.086	39.726	43.856			0	
EAR HYD. FL	OR m3 DAY	89,630	1.086	91,954	89.263	36.547 91.954	7,854	545	7,30
IN. FLOW	m3/DAY	14,341	1.085	15,427	15.427	15,427	7.854	545	7,308
\$\$	■g. L	882	2,350	880	20	70 20	545 20	20	
55	tg 'day	31.627	2.552	34,976	877	731	157	11	145
22	mg/L	667	500	638	14	1/	14	14	148
ss 00 ₅	16/617	23.928	543	25.273	614	512	110		102
005	■g/L	762	4.800	820	20	10	20	20	20
	hg/day	27,317	5,213	32.561	877	731	157	11	148
.0.				 	 	6.9			
				 		3.0			

			$\overline{}$	7			
STREAM NO.		(10)		(12)	(13)	(14)	(15)
AVERAGE FLOW	m ³ /day	46.396	43.217	3,179	2,119	1 22	
PEAK FLOW	a ³ /day	58,404	58,404			1,060	1,728
MINIMUM FLOW	m3/day						1,850
DES160 755	\$	10	1.0	1.0	+		
DESIGN TSS	mg/L	10,000	10,000		1.5	.07	<u> </u>
DESIGN TSS	kg/day	463,960	1	10,000	14.500	723	21
DESIGN YSS	\$	0.7	432.170	31,739	30,974	765	37
DESIGN YSS	mg/L		0.7	0.7	1.02	.05	
		7,000	7,000	7.000	10.200	506	15
DESIGN YSS	FE/651	324,772	302,519	22,217	21,681	536	28

WESTON INTERNATIONAL, INC.
IN ASSOCIATION WITH STANLEY CONSULTANTS, INC.,
SIGMA CONSULTING ENGINEERS
MRM CONSULTING ENGINEERS CO., LTD

IRBID WATER SUPPLY, SEWERAGE, STORM DRAINAGE AND SOLID WASTE DISPOSAL PROJECT

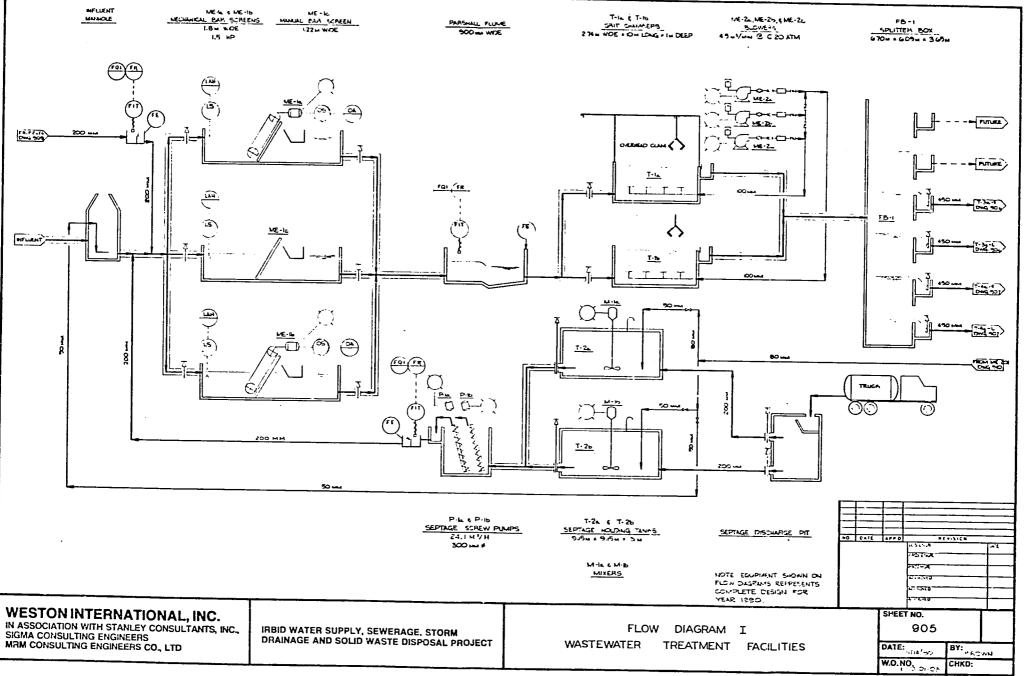
MASS BALANCE - SCHEDULE II (YR. 2000) WASTEWATER TREATMENT FACILITIES

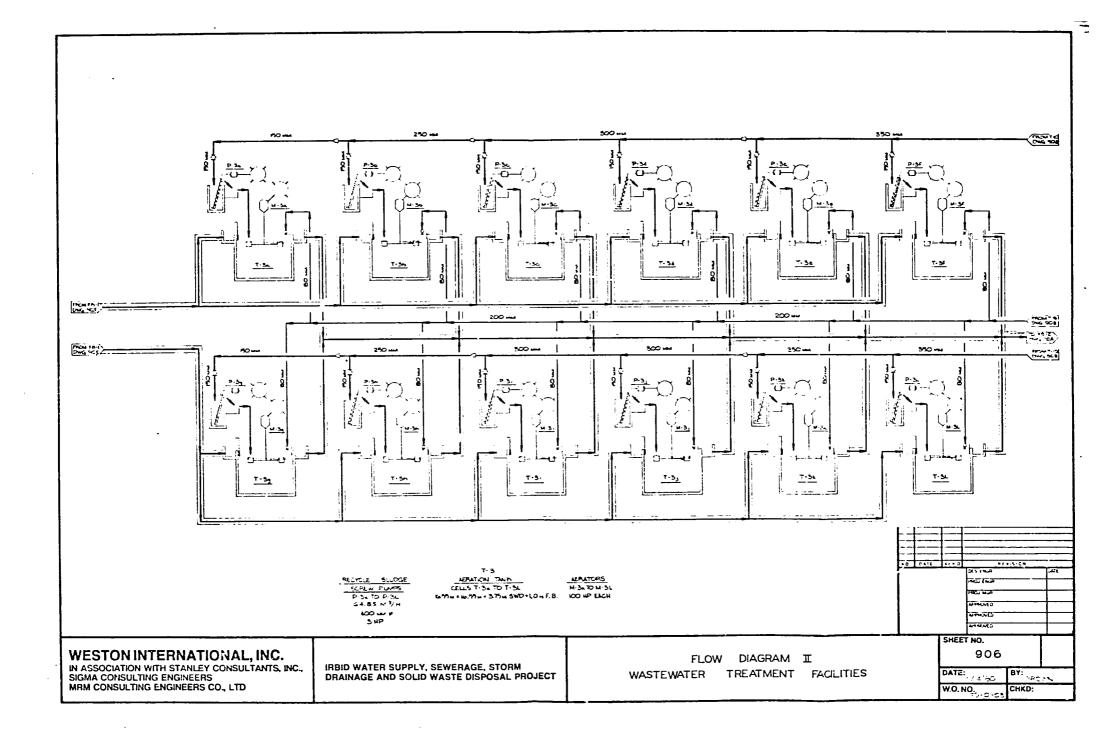
SHEET NO. 902 DATE: BY: W.O. NO

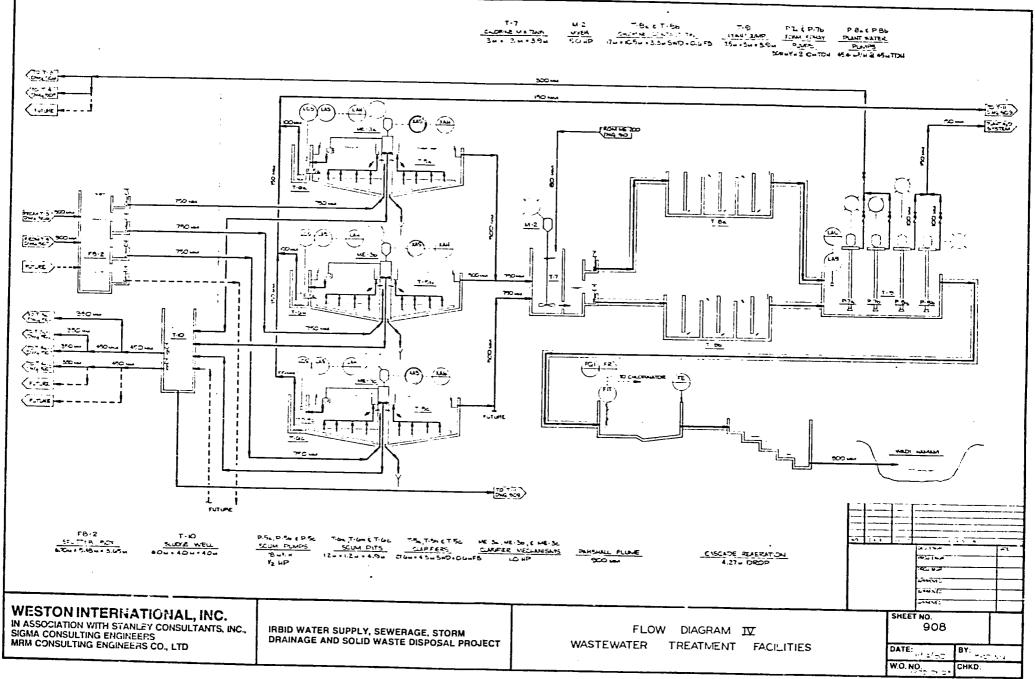
W.O. NO

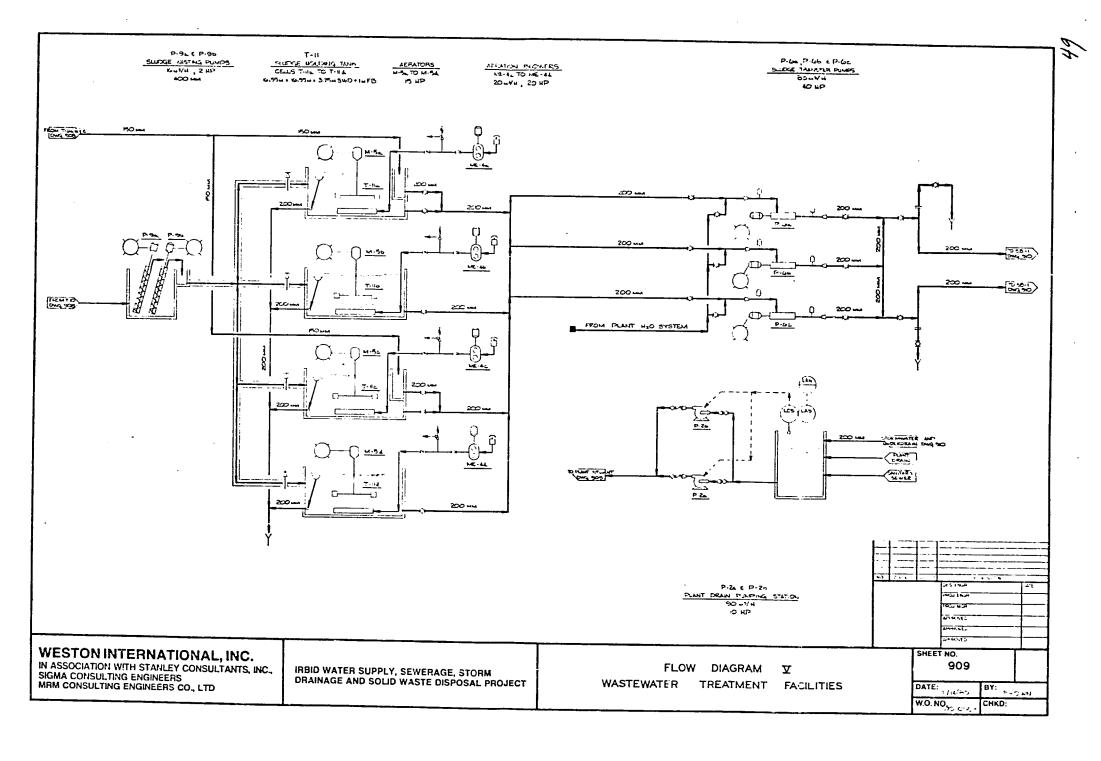
CHKD:

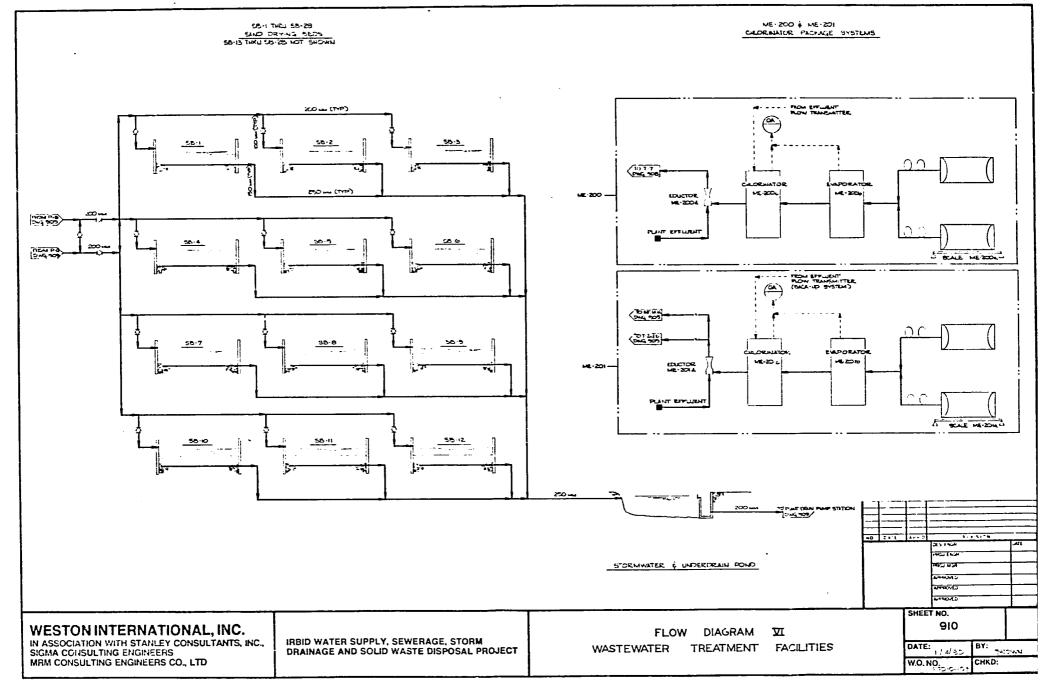
LINES	PIPING					
	THE INTO	PUMPS		EQUIPMENT NUMBERING	INSTRUMENTS & ELECTRICAL	
PROCESS LINE AUXILIARY AND ELECTRICAL LIN	E -1- EDUCTOR OR EJECTOR	THE CENTRIFUGAL PUMP	B-1 C-1 F-1 FB-1 GF-1 B-1	BASIN LACOON CONVETTAGE COUPPERT COMPRESSOR BLOOGR FLOW POLITY CRAFTLY FILTER WISTER ALRADOR	OF HOTE - 2 INSTRUMENT - LOCALLY MOUNTED INSTRUMENT - BOARD MOUNTED (LOCAL	INSTRUMENT TERMINOLOGY
PROBABLIC LINE SONIC OR BADIAL CS	RAMENT LINE —— ECCENTRIC REDUCER HOSE COMMECTION HOSE COMPETION BLIND FLANG GCUPPERT INSULATED	O-G DIAPHAGE PURP O-G- VACCOR PURP O-G- PROCRESSIVE CAVITY PURP	P-1 P-1 PF-1 T-1	OTHER MECHANICAL EQUIPMENT MAMMOLE PLAN TARK TARK TARK TARK TARK TARK TARK TARK	INSTRUMENT - BOARD WOMITED (LECTAL) INSTRUMENT - BOARD WOMITED (WAIN PAMEL) INSTRUMENT - BACK OF MAIN PAMEL INSTRUMENT - DUAL ELEMENT IN	C COMMUNITY CONTROL CO
VALVE BODIE	ES EQUIPMENT MEAT TRACED / Y ORAIN ====================================	C SCREEN PARP	н.	LINE DESIGNATION	EQUIPMENT NER SUPPLIED DEVICE	L LITTL LIGHT (PILET) LND (MISTOR) LND (MISTOR) LND (MISTOR) PRISONE PRISONE PRISONE (MISTOR) LND (MISTOR) LN
-coo- ALE BUTT AUTAE -coo- PUTT AUTAE -coo- CTORE AUTAE B. I		VERTICAL CERTRIFUGAL PUMP VERTICAL TURBICS PUMP SPECIAL EQUIPMENT	ST -	SLUDGE SVETEMBATANT FILTRATE ILTER BACEBASH TYPASSES OVERFLOWS KLUB RAINS	COMPLEX INTERLOCK (BACKWASH) - ON - SIMPLE INTERLOCK	A MAINTENENTY RECORDED RECORDED STATES OF THE STATE STATES OF THE STATES
PLUG VALVE	PIPE UNION SHOCK ABSORBER OR SURGE LINE CAP	SCREW CONVEYOR	SN - II	UILDING SANITARY TILLITY WATER OF SIZE TIPE OF FLOR OF 1100 MAI FLOR (GPH) MAI MANAGER	PURCE 1 10 P TILLURITERIES TO PROMULE COMPUTER	1 19650 Mill Mill Mill 2 1951100 Mill 2 1951100 Mill 2 5)
SUM DIECE VALVE	YALVE SILENCER	COMMINUTOR	OI - O PR - PI AM - AI ML - ME LW - LI	IR TYTECH DLYMER LUM THANDOL ME	PI PRESSURE (VACAME) GAGE P S I BANGE	1 THE FRESHMEN ASSESSMENTATIONS AND THE SET PACKED BETSEME OF FRESHMEN AND THE SET PACKED BETSEME OF THE SET PACKED BETSEME OF THE SECONDARY ASSESSMENT OF THE SECONDARY A
SAFETY MELIEF VAL	GATES	T YARIABLE SPEED EXMPLTS T YARIABLE SPEED MOTOR	AM CA	ERIC DIDRIDE LORINE MODELE STILLE STILLE ACTUATORS	PRESSURE GAGE 9 SEAL	
PRESSURE MEDUCING FLAP VALVE FLAP CONTROL VAL	TALVE STOP PLATE	The MARIABLE SPEED PUMP		TOR OPERATED VALVE	OPERATING LIGHT COLOR UR GO: GRAPHIC DISPLAY	ALGAL BASEAST OF THE SELLOW STREET ARTESTATION ARTESTAT
DIAPHRAGE VALVE DIAPHRAGE VALVE DIAPHRAGE VALVE PET COCK VALVE	AIR MOVING EQUIPMENT	PULSATION CAMPERER ABBREVIATION	-ोंगे ल	FLOW ELEMENTS		## ## ## ## ## ## ## ## ## ## ## ## ##
CUSHIDNED SPING OF TELESCOPING VALVE	TE DISTRICT COMPRESSOR	I A S - INSTRUMENT AIR SUPPLY N C - VALVE ROWALLY CLOSED N O - VALVE ROWALLY OFTE		IFICE ITURI FLOW CLEMENT W ELEMENT (* SIZE IN INCHES)		4 ALL INTERPRETATION STATEMENT AND AND POPULATION OF CONTINUENT SECRET OF ANGELIES STANDARDS FOR THE CONTINUENT SECRET OF THE CONTINUENT SECRET SECRE
MOTE: ALL VALVE BODIES OF DIMENSISE MOTED	* FM (ARTAL)		- FLU	13		S LECATION OF LECAT FRANCE OF MORE THAN DOC IS WELL OCC - MOINT CONTROL CINTER OF - PRESSAND FRANCE OF - CHRESTO FRANCE OF - SACOUN FRANCE
SIGMA CO	ON INTERNATIONAL, INC. HATION WITH STANLEY CONSULTANTS, INC., DISULTING ENGINEERS ISULTING ENGINEERS CO., LTD	IRBID WATER SUPPLY, SEWERAGE, STORM DRAINAGE AND SOLID WASTE DISPOSAL PROJECT	ст		LEGEND INSTRUMENTATION SYMBOLS	SHEET NO. 904 DATE: BY:











W.O. NO

CHKD:

